In the Claims:

1. (Currently Amended) A ~~M~~method for producing hydrogen, electricity and at least one hydroprocessed product from a hydrocarbonaceous feedstock comprising at least a fraction which has a boiling point range ~~which is~~ the same as or higher than the boiling point range of the hydroprocessed product ~~to be produced~~, which method comprises:

a) subjecting the hydrocarbonaceous feedstock to a treatment with hydrogen in the presence of a supported catalyst under conditions effective to produce a hydrotreated feedstock comprising a hydroprocessed product, ~~which~~ said hydrogen ~~has been~~ being produced at least partly from a fraction of the hydrotreated feedstock having a boiling point range different from the boiling point range of the fraction of the hydrocarbonaceous feedstock from which the hydroprocessed product ~~will be~~ is produced, or from at least part of said hydroprocessed product~~,~~;

b) separating the hydroprocessed product from hydrotreated feedstock when hydroprocessed product is to be recovered; and,

c) subjecting part or all of the remaining hydrotreated feedstock and the hydroprocessed product if it is not ~~to be~~ recovered to a treatment to produce hydrogen, recycling at least a part of the hydrogen to step a), and subjecting part or all of the hydrogen not used for ~~the treatment with hydrogen~~ step a) to a treatment to produce electricity, or subjecting part of the hydrotreated feedstock and the hydroprocessed product if it is not ~~to be~~ recovered to a treatment to produce electricity and at least part of the remainder to a treatment to produce hydrogen and recycling at least a part of the hydrogen to step a).

2. (Previously presented) The method of claim 1, in which use is made of feedstocks ranging from those having an initial boiling point of about ambient to those having a final boiling point of about 650 °C.

3. (Previously presented) The method of claim 2, in which use is made of feedstocks having a boiling point range such that their 90% boiling point lies in the range between about 400°C and about 600 °C.

4. (Previously presented) The method of claim 1, in which use is made of feedstocks having a sulphur content of not more than 5 %wt.

5. (Previously presented) The method of claim 1, in which a hydrocarbonaceous feedstock is used containing between about 5 %wt and about 40 %wt of material having a boiling point range which is the same as or higher than the boiling point range of the hydroprocessed product to be produced.

6. (Previously presented) The method of claim 5, in which the feedstock contains between about 5 %wt and about 40 %wt of material having a boiling point above the final boiling point of the hydroprocessed product.

7. (Previously presented) The method of claim 1, in which kerosene and/or gas oil are recovered as hydroprocessed product(s) from the hydrotreated feedstock.

8. (Previously presented) The method of claim 1, in which part or all of the non-recovered material from the treatment with hydrogen is subjected to a catalytic oxidation process which produces hydrogen and carbon (di) oxide.

9. (Previously presented) The method of claim 8, in which the catalytic oxidation process comprises a catalytic partial oxidation process.

10. (Previously presented) The method of claim 8, in which hydrogen not used in the hydrotreatment step is used at least partially to produce electricity by feeding it to a fuel cell which is operated to deliver electricity and water (steam).

11. (Previously presented) The method of claim 10, in which the electricity in excess of that needed for the utilities of the process is produced from excess hydrogen.

12. (Previously presented) The method of claim 10, in which at least part of the steam needed in the hydrogen manufacturing unit is provided by the fuel cell.

13. (Currently amended) The method of claim 1, in which said catalytic oxidation process comprises a watergas-shift process, and in which kerosene and/or gas oil, are produced from no feedstocks other than the hydrocarbonaceous feedstock and water used in the watergas-shift ~~step~~ process.

14. (Previously presented) The method of claim 1, in which hydrogen sulphide generated by the treatment with hydrogen is converted into elemental sulphur by conventional means.

15. (Canceled)

16. (Currently amended) The method of claim ~~15~~31, in which use is made of a catalyst containing zeolite beta as active component in the treatment with hydrogen.

17. (Currently amended) The method of claim ~~16~~32, in which the zeolite beta-based catalyst is capable of converting at least 90 %wt per pass of the fraction to be treated to obtain the hydroprocessed product.

18. (Currently amended) The method of claim ~~15~~31, in which the treatment with hydrogen is carried out at a temperature between about 100°C and about 550 °C.

19. (Currently amended) The method of claim ~~15~~31, in which the treatment with hydrogen is carried out at a pressure of up to 400 atmospheres.

20. (Currently amended) The method of claim 10, in which the fuel cell ~~step~~ is operated in such a way that it delivers excess electricity.

21. (Currently amended) The method of claim 9, in which the catalytic partial oxidation step and the fuel cell step are operated in such a way that they ~~generated~~ generate the internal needs on hydrogen and electricity for the process.

22. (Currently amended) The method of claim 9, in which the hydrogen generated by the catalytic partial oxidation step ~~has been~~ is produced at least partly from hydrocarbons containing at most 4 carbon atoms present in the hydrocarbonaceous feedstock or as produced during the hydrotreatment step.

23. (Previously presented) The method of claim 22, in which the feedstock for the catalytic partial oxidation step consists of hydrocarbons having about 4 or less carbon atoms.

24. (Currently amended) The method of claim 1, in which hydrogen is separated off from the hydrotreated feedstock and from the hydroprocessed product if the latter is not ~~to be~~ recovered prior to the hydrogen manufacturing step.

25. (Previously presented) The method of claim 1, in which use is made of feedstocks having a sulphur content below 3 %wt.

26. (Previously presented) The method of claim 8, in which the catalytic oxidation process comprises a watergas-shift process.

27. (Currently amended) ~~The method of claim 1, in which hydrogen is produced~~ A method for producing hydrogen, electricity and one or more hydroprocessed product from a hydrocarbonaceous feedstock, the method comprising:

a) exposing the hydrocarbonaceous feedstock to hydrogen in the presence of a supported catalyst under conditions effective to produce hydroprocessed product;

b) separating the hydroprocessed product from hydrotreated feedstock when hydroprocessed product is to be recovered;

c) subjecting part or all of the remaining hydrotreated feedstock and the hydroprocessed product if it is not recovered to a treatment to produce hydrogen and subjecting part or all of the hydrogen not used for step a) to a treatment to produce electricity, or subjecting part of the hydrotreated feedstock and the hydroprocessed product if it is not recovered to a treatment to produce electricity and at least part of the remainder to a treatment to produce hydrogen; and

d) subjecting part or all non-recovered material from step a) to a watergas shift process comprising catalytic oxidation which produces hydrogen and carbon dioxide and recycling at least a part of the hydrogen to step a), the hydrogen in step a) being produced from no

feedstocks other than the hydrocarbonaceous feedstock and water used in the watergas-shift step process.

28. (Previously presented) The method of claim 1, in which said supported catalyst converts at least about 65 %wt per pass of said fraction of the hydrocarbonaceous feedstock having a boiling point range the same as or higher than the boiling point range of the hydroprocessed product.

29. (Previously presented) The method of claim15, in which the treatment with hydrogen is carried out at a temperature between about 250°C and about 450 °C.

30. (Previously presented) The method of claim 15, in which the treatment with hydrogen is carried out at a pressure of between about 10 and 200 atmospheres.

31. (New) A method for producing hydrogen, electricity and one or more hydroprocessed product from a hydrocarbonaceous feedstock, the method comprising:

a) exposing the hydrocarbonaceous feedstock to hydrogen in the presence of a supported catalyst, the supported catalyst and the conditions being effective to convert to the hydroprocessed product at least about 50 %wt per pass of a fraction of the hydrocarbonaceous feedstock having a boiling point range the same as or higher than the boiling point range of the hydroprocessed product, the hydrogen being produced at least partly from a fraction of the hydrotreated feedstock having a boiling point range different from the boiling point range of the fraction of the hydrocarbonaceous feedstock from which the hydroprocessed product is produced, or from at least part of the hydroprocessed product;

b) separating the hydroprocessed product from hydrotreated feedstock when hydroprocessed product is to be recovered; and

c) subjecting part or all of the remaining hydrotreated feedstock and the hydroprocessed product if it is not recovered to a treatment to produce hydrogen, recycling at least a part of the hydrogen to step a), and subjecting part or all of the hydrogen not used for step a) to a treatment to produce electricity, or subjecting part of the hydrotreated feedstock and the hydroprocessed product if it is not recovered to a treatment to produce electricity and at least part of the remainder to a treatment to produce hydrogen and recycling at least a part of the hydrogen to step a).